

Finally, it must be pointed out that in this experiment the hydraulic entrance length was about 19 hydraulic diameters. At higher Reynolds number flow than we have considered here, a longer entrance length is needed to achieve fully developed turbulent flow.³ Furthermore, Eq. (1) is derived by neglecting the magnetic and thermal entrance effects; local heat transfer coefficient measurements are needed in future research to justify this assumption.

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- ζ = normal to body surface
- S = stagnation point of potential flow
- U = velocity of potential flow
- U_m = meridional component of U
- U_ϕ = circumferential component of U
- U_∞ = velocity of undisturbed flow
- α = angle of incidence of the body

Introduction

THE exact prediction of the position of boundary-layer separation for bodies at angle of attack is a problem of great practical importance in aircraft design. Boundary-layer calculations based on one of the common simplifications such as similarity, small crossflow, small perturbation give only approximate solutions of this problem which are not always satisfactory. In the present method, no simplification of the boundary-layer equations is introduced. The complete three-dimensional laminar boundary-layer equations are solved numerically by an implicit finite difference technique.

Recently, Blottner and Ellis¹ and Wang² also presented methods based on finite difference concepts. A discussion of separation patterns over inclined bodies of revolution was given by Wang.³ Both authors use coordinate systems which are fixed to the body geometry. To extend the calculation over the entire body surface a separate quasi two-dimensional calculation process along one line of symmetry is necessary to specify initial boundary-layer profiles along this line. The application of both methods is limited to simple bodies of revolution like prolate spheroids or elliptic-paraboloids where the inviscid flow data can be obtained analytically.

In the present method a streamline coordinate system is introduced. The coordinates are represented by the streamlines and potential lines of the outer inviscid flow. Using streamline coordinates the extension of the numerical boundary-layer calculation over the entire body surface is a straightforward process. No transformation from one into another coordinate system is necessary. A finite difference scheme is chosen which permits one to include the lines of symmetry of the flow into the calculation process. No initial data along the lines of symmetry have to be specified. The outer inviscid flow is calculated numerically by a singularity method which has been developed by the author.⁴ Therefore this method is applicable to bodies of revolution with arbitrary cross-sections. To determine the position of boundary-layer separation the condition of numerical stability (Courant-Friedrich-Levy condition) serves as a useful criterion.

Governing Equations

Figure 1 describes the problem and gives the notation in a streamline coordinate system: the rectilinear coordinate system ξ, η, ζ is oriented in the direction of streamlines, equipotential lines, and normal to the surface, respectively. The corresponding velocity components in these directions are, u, v, w , whereas U is the velocity of the outer inviscid flow, U_∞ is the undisturbed mainflow velocity, and α the angle of attack. Here the velocity component u , which is parallel to the streamlines of the outer flow, is the primary velocity and the velocity component v normal to the streamlines gives the secondary flow in the boundary layer. All lengths are made dimensionless with the

Three-Dimensional Laminar Boundary Layer over a Body of Revolution at Incidence and With Separation

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Nomenclature

- x, r = cylindrical coordinates
- L = total length of body
- ξ, η, ζ = system of rectangular coordinates, oriented with regard to the potential flow
- ξ = in direction of streamlines
- η = in direction of equipotential lines

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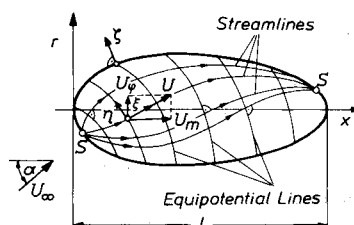


Fig. 1 Flow around a body of revolution at incidence.

total body length L , all velocities with U_∞ , and pressures with ρU_∞^2 , where ρ is the density. The quantities ζ and w are multiplied in addition by $Re^{1/2}$, where Re is the Reynolds number ($Re = U_\infty L/\nu$) and ν the kinematic viscosity.

The boundary-layer equations for steady three-dimensional laminar incompressible flow in curvilinear coordinates in dimensionless form are:

Equation of continuity

$$\frac{\partial u}{h_1 \partial \xi} + \frac{\partial v}{h_2 \partial \eta} + \frac{\partial w}{\partial \zeta} - K_1 u - K_2 v = 0 \tag{1}$$

Equation of momentum in ξ direction

$$u \frac{\partial u}{h_1 \partial \xi} + v \frac{\partial u}{h_2 \partial \eta} + w \frac{\partial u}{\partial \zeta} - K_2 uv + K_1 v^2 = -\frac{\partial p}{h_1 \partial \xi} + \frac{\partial^2 u}{\partial \zeta^2} \tag{2}$$

Equation of momentum in η direction

$$u \frac{\partial v}{h_1 \partial \xi} + v \frac{\partial v}{h_2 \partial \eta} + w \frac{\partial v}{\partial \zeta} - K_1 uv + K_2 u^2 = -\frac{\partial p}{h_2 \partial \eta} + \frac{\partial^2 v}{\partial \zeta^2} \tag{3a}$$

The boundary conditions are:

$$\begin{aligned} u = v = w = 0 & \text{ at } \zeta = 0 \\ u = U, v = w = 0 & \text{ as } \zeta \rightarrow \infty \end{aligned} \tag{3b}$$

The local curvature parameters K_1, K_2 are defined as follows:

$$K_1 = -\frac{1}{h_1 h_2} \frac{\partial h_2}{\partial \xi}; \quad K_2 = -\frac{1}{h_1 h_2} \frac{\partial h_1}{\partial \eta} \tag{4}$$

In Eqs. (1-4) h_1 and h_2 are the metric coefficients such that $h_1 d\xi$ is the actual differential length along streamlines and $h_2 d\eta$ is the actual differential length along equipotential lines. In streamline coordinates the term h_1 is defined by:

$$h_1 = 1/U \tag{5}$$

Method of Solution

The differential Eqs. (1-3b) represent a mixed initial value and boundary value problem. Before the actual numerical boundary-layer calculation can start initial boundary-layer profiles near the front stagnation point as well as potential flow data at the outer edge of the boundary layer have to be specified. For the computation of initial boundary-layer profiles along equipotential lines near the front stagnation point the well-known three-dimensional stagnation point boundary-layer solution of Howarth⁵ is used.

The potential velocity distribution on the body surface is calculated by a singularity method⁴ giving the flow quantities in a large number of discrete surface points. It is possible to calculate the potential velocity components in arbitrary surface points by means of a spline-interpolation process.

Knowing the surface velocity components in meridional direction (U_m) and in circumferential direction (U_ϕ) (Fig. 1), one obtains the surface streamline equation in the form:

$$U_\phi/U_m = r d\phi/ds \tag{6}$$

where r is the radius of the body at station x , ϕ is the circumference angle, and ds is the arc length along meridians. Equation (6) is integrated numerically by the Runge-Kutta method. The velocity potential Φ is determined by

$$\Phi = \int_{\xi_0}^{\xi} U h_1 d\xi \tag{7}$$

with integration along streamlines. The equipotential lines are simply defined by the condition $\Phi = \text{constant}$. With Eqs. (6) and (7) a complete set of streamline coordinates can be calculated. But the mesh sizes formed by the stream- and equipotential lines may not be arbitrary with respect to the three-dimensional finite difference method. Hall⁶ has extended the implicit finite difference procedure of the Crank-Nicholson type to the three-dimensional case. In contrast to the two-dimensional case, this method is not always stable. A numerical stability condition, namely the Courant-Friedrich-Levy condition, must be satisfied through the boundary layer.

For the finite difference scheme investigated by Hall, which

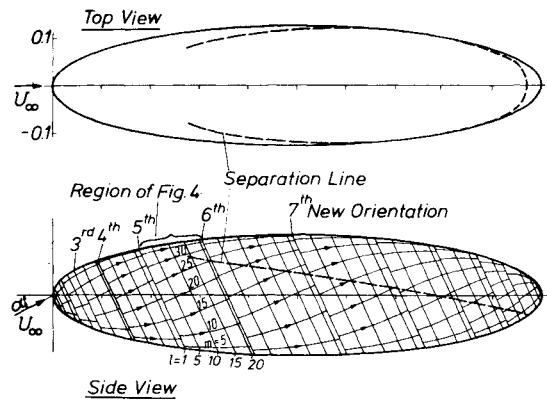


Fig. 2 Streamline net with separation line for an ellipsoid of revolution of axis ratio $a/b = 4$ at $\alpha = 15^\circ$ angle of attack, $l = \text{number of equipotential line}$, $m = \text{number of streamline}$.

is used in the present method, the stability condition takes the form:

$$\left| \frac{v h_1 \Delta \xi}{u h_2 \Delta \eta} \right| \leq 1 \tag{8}$$

This condition is based on the concept of the zone of dependence. If the ratio of mesh sizes, $h_1 \Delta \xi / (h_2 \Delta \eta)$, in Eq. (8) is equal to one or is smaller than unity, the mesh sizes are favorable with respect to the stability condition.

A mesh of streamlines and equipotential lines with such controlled mesh sizes is plotted in Fig. 2 for an ellipsoid of revolution of axis ratio $a/b = 4$ at angle of attack $\alpha = 15^\circ$. The streamlines have to be reorientated several times along equipotential lines. Flow data are transformed from one system into the neighboring one by a simple interpolation process along the corresponding equipotential lines.

With known potential flow in all netpoints of the coordinate system and with initial boundary-layer profiles in the vicinity of the stagnation point, the numerical solution of Eqs. (1-3b) can start. The differential quotients are approximated in the usual way by finite differences around the central point of the difference scheme. The method is implicit in ζ direction and involves the solution of simultaneous linear algebraic equations with tri-diagonal coefficient matrices. In correspondence with Hall's method, the three boundary-layer equations are solved by an iteration process.

The computation marches from netpoint to netpoint along equipotential lines and streamlines including both lines of symmetry.

In Fig. 3 an example of the boundary-layer calculation is given for the same ellipsoid as in Fig. 2 and for the angle of incidence

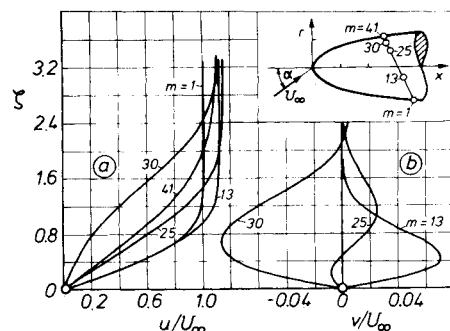


Fig. 3 Velocity distribution of the three-dimensional boundary layer on an ellipsoid of revolution of axis ratio, $a/b = 4$, at angle of attack $\alpha = 15^\circ$; a) Primary flow profiles, u/U_∞ , in direction of outer flow streamlines, b) Secondary flow profiles, v/U_∞ , normal to the direction of outer flow streamlines. The profiles are given for potential line $l = 13$ of Fig. 2 at streamline stations m from Table 1.

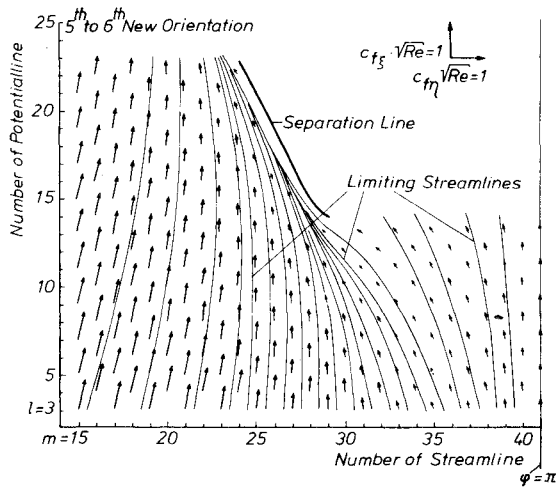


Fig. 4 Vectors of the local skin friction coefficient c_f and limiting streamlines. Beginning of separation between the 5th and 6th new orientation in Fig. 2, that is between $x/L = 0.251$ and $x/L = 0.385$ along the windward symmetry line.

$\alpha = 15^\circ$. Both the profiles of the primary velocity, u , and of the secondary velocity, v , are plotted against the dimensionless distance ζ from the wall for five and three different streamlines, respectively, the numbers of which are given in Fig. 2. The area covered is close to the separation line of Fig. 2. In the region of maximum negative secondary flow (point $m = 30$ in Fig. 3) the u -profiles have a point of inflection corresponding to a minimum of wall shearing stress in this direction.

Separation

The numerical boundary-layer calculation can be extended over the body surface until a point is reached, where the stability condition Eq. (8) is violated. Figure 4 represents an example of the numerical calculation again for the ellipsoid of axis ratio $a/b = 4$ at an angle of attack of $\alpha = 15^\circ$ (Fig. 2). In a small region which is marked in Fig. 2 the distribution of the vector of the local skin friction coefficient c_f is plotted as defined by

$$\frac{1}{2}c_f = \frac{\tau_o}{\rho U_\infty^2} = \frac{1}{(Re)^{1/2}} \left[\left(\frac{\partial u}{\partial \zeta} \right)^2 + \left(\frac{\partial v}{\partial \zeta} \right)^2 \right]^{1/2} \quad (9)$$

with τ_o as shearing stress at the wall.

The limiting streamlines are calculated by integration of the directions of the c_f -components. These wall streamlines run into one line forming an envelope. Near this envelope a maximum of reversed secondary flow in connection with a decrease of the primary velocity components occurs (see Fig. 3). The boundary-layer thickness reaches a steep maximum in this region. The computation can be extended downstream of the first numerical instability point always marching along equipotential lines until numerical instability occurs. The so determined instability line corresponds to the envelope of the limiting streamlines and is plotted in Fig. 2. This line is interpreted as the separation line of the free vortex layer type in the sense of Maskell⁷ and Wang.³ The separation line ends at the windward symmetry line of the potential flow, where reversed flow occurs in the boundary layer.

Table 1 Streamline station coordinates

m	x/L	$\phi [^\circ]$
1	0.360	0
13	0.322	71
25	0.277	122
30	0.264	141
41	0.254	180

Similar results have been obtained for numerous bodies of revolution with different axis ratios and angles of attack.⁸ The present numerical method has also been tested for the simple cases of a sphere and a semi-infinite cylinder in cross flow. In both cases very satisfactory results with respect to the location of the separation point or separation line have been obtained with analytical methods.

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Penny-Shaped Crack in a Linear Viscoelastic Medium under Torsion

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I. Introduction

IT is well known that to solve a viscoelastic boundary value problem that involves the boundary conditions of mixed type, the classical correspondence principle of obtaining the viscoelastic solution from the associated elastic solution is, in general, no longer applicable. Graham¹ has proposed a correspondence principle for problems with time-dependent boundary regions and has applied it² to solve the problems of a penny-shaped crack subjected to a tension normal to the plane of the crack. Ting³ has developed a technique of solving problems with moving boundaries and has applied it to obtain the contact stresses between an axisymmetric rigid indenter and a viscoelastic half space. Present authors⁴ have applied this method to solve the problems of a penny-shaped crack in a viscoelastic medium under shear.

In the present Note we solve the related problem of a penny-shaped crack in a linear viscoelastic medium under torsion. Expressions for the stress distribution in the plane of the crack, displacement over the surface of the crack, and the stress intensity factor are given in the closed form. These quantities

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